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A Review of Odour Discharges and Control in Rendering and Related Activities Ron Pilgrim, Air Quality Manager, Kingston Morrison Limited

Introduction

Rendering inedible raw materials gives valuable by-products and avoids significant disposal problems such as costly land filling. Rendering involves thermal or thermo-mechanical breakdown of meat, fish, and poultry materials into solids, fat or oil, and water; separation of the components; drying of solids; and refining of fat. The contained solids and fat in wastewater are occasionally extracted in a wast evaporator. Most plant now employs 'low temperature rendering' (LTR). LTR is the thermo-mechanical disintegration and phase separator of raw material components typically at 90-95°C, with product drying following the rendering/reduction (wet processing) stage. If the thermo-accompanied by and/or followed by evaporative drying. While low temperature rendering has lower air pollution point than high temperature rendering, its nuisance potential can still be high. Blood is normally heat coagulated, blood solids separated blood water and dried by application of heat, and blood water discharged to the drain.

Odorous Contaminants

A significant consequence of rendering and drying activities is the discharge to atmosphere of odorous contaminants (pollutants), following classes of contaminants may be generated to a greater or lesser degree from rendering and blood drying operations. Sulphide disulphides such as hydrogen sulphide and dimethyl sulphide, mercaptans such as methyl mercaptan, and other odorous sulphur component ammonia, and volatile amines such as methyl amine and trimethyl amine, and other odorous compounds of nitrogen; hydrocarbons partially oxidised hydrocarbons such as the aldehydes 2-methyl butanal and 3-methyl butanal; and volatile carboxylic acids such as the aldehydes 2-methyl butanal and 3-methyl butanal; and volatile carboxylic acids such as the acids butyric acid; and pyrolysis products of paunch and gut contents, protein, connective tissue, and fat. Collectively, these and contaminants are termed odorous compounds (odours). Specific compounds present and their discharge concentrations depend on material type and quality, processing method (especially rendering and drying temperature), and discharge control equipment efficiency.

Low temperature rendering vessel temperatures are not high enough to degrade raw material and cause odour generation, but are sufficient drive off volatile contaminants resulting from putrefaction. In high temperature rendering, some reduced sulphur compounds such hydrogen sulphide, as well as resulting from putrefaction, are generated in high concentration from the thermal breakdown of skin, wool, and hooves. Partially oxidised hydrocarbons such as the aldehydes 2-methyl butanal and 3-methyl butanal and volatile carboxylic such as fatty acids, are all thermal breakdown products of fat. Overheating or over-drying meal (which is abnormal operation), especial the meal fat content is too high, will generate "burnt" odours and sulphides. The presence of gut and paunch contents in meal cater generate 'burnt grass' odours in direct-fired driers. The potential for over-drying is the same for low temperature and high temperature is not well controlled. Likewise, processing of 'stale' raw material could result in the discharge of malant at any stage in the rendering process. Processing sour blood, and burning blood during drying, generates objectionable odour.

Minimising Generation/Discharge of Odorous Contaminants

Environmentally acceptable and cost-effective rendering and blood drying requires good quality raw materials, well designed and mainly processes, and good management. Ensure that raw materials processed are of good quality; operate processing equipment to minimum generation of objectionable odours; contain all significant process odour sources then ventilate to odour control equipment; maintain a housekeeping to minimise background odour; and ventilate processing buildings to minimise build-up of contaminants and to maintain satisfactory workplace environment. Not only is such a program necessary to minimise the discharge to atmosphere of odorous contaminant and preventing over-loading of odour control equipment, but proper processing of good quality raw material maximises product quality.

Raw Material Quality. Raw material quality definitions were developed by the Department of Health in 1985. These were frequently applies as conditions of Clean Air Licences for rendering processes. Many regional councils have applied them or variants as conditions of discharge permits under the Resource Management Act. A current definition of "good quality" inedible soft offal is:

(a) Meat material which is cut and washed substantially free of paunch material and is rendered within eight hours from kill providing s material is maintained at a temperature less than 25 degrees Celsius, and in any case does not have an objectionable odour; or

(b) Meat material which is cut, washed, and maintained as above which is adequately stabilised (preserved) as soon as possible but not be than eight hours from kill by cooling the whole mass to less than 20 degrees Celsius or by treating with acid to ensure the whole maintains a pH less than (more acid than) 4.5, or preserved by equivalent means, and is processed within 24 hours from kill, and in case does not have an objectionable odour. pH shall be determined from the liquid derived from the offal.

The quality of other raw materials, including DAF sludge, are also defined. Regional councils may change requirements depending on material type and processing method. The above definition of soft offal is conservative. I now believe that temperature stabilisation, desirable, is not as important as previously thought. Washing cut paunch and gut material with hot water to substantially remove bacterial enzymes (and grass material) gives substantial benefits over no washing, therefore, the definition can be amended as follows:

(a) Soft offal which is cut and washed substantially free of paunch and gut material and is rendered as soon as practicable but in any within ten hours from kill, and does not have an objectionable odour.

<u>Containment of Odorous Contaminants.</u> Discharges from high temperature rendering equipment such as batch melters, continuous coole and presses; from LTR render vessels, presses, decanters, liquid phase tanks and screens, etc; from blood coagulation equipment, drying equipment; and in some cases meal and blood mills; should be contained or hooded and ventilated (usually through a condensed appropriate odour control equipment. Material conveyors prone to significant fugitive odour discharge should be contained or hooded ventilated to odour control equipment. Some processing equipment is difficult to contain or hood and ventilation of processing building odour control equipment may be the only option especially for plant located in sensitive areas. Processing Building Ventilation Air Control. Ventilation of processing buildings at 10-15 air changes/hour or more should provide an acceptable working environment, will minimise condensation of steam on cool internal surfaces, and will avoid build-up of odorous contaminants which can escape when access doors are opened. If raw material quality, process containment, and housekeeping, is good and the locality is a secape when access doors are opened. If raw material quality, process containment, and housekeeping, is good and the locality is not highly sensitive or topographically complicated, discharge of ventilation air through a chimney sufficiently high to avoid buildings or elevated ground building downwash and to maximise dispersion may be acceptable. Discharged air must not impinge on high buildings or elevated ground down wind. The alternative is treatment of ventilation air before discharge. Processing buildings should be designed (including minimising volume). Volume) to enable retro-fitting a controlled ventilation air system if it proves necessary.

Contensers. Process gases and fugitive discharges having significant water content should be routed to condensing equipment. Gas streams containing a high proportion of air (and possibly excessive particulates) can be treated in spray (direct) condensers but this produces contaminated cooling water. Re-circulation of cooling water through a heat exchanger is necessary for heat recovery, or to avoid contaminated cooling water. contamination of evaporative cooling towers. Other gas streams can be treated in an indirect (shell & tube) condenser which has the added advantage of keeping foul condensate and cooling water separate. Foul condensate and spray condenser blow-down water temperature should b_{e} as low as practicable (preferably less than about 40°C) and discharge to an impervious drain.

Internet of Non-condensable Gases. A variety of equipment is available to substantially destroy (with varying degree of success) odorous non-condensable Gases. A variety of equipment is available to substantially destroy (with the high equipment and biofiltration. Choice of method (and the gases. The principal methods used in New Zealand are incineration, chemical scrubbing, and biofiltration. Choice of method (and the gases. The principal methods used in New Zealand are incineration, chemical scrubbing, and biofiltration, choice of the gases. method (and satisfactory performance) depends on nature and volume of non-condensable gases, required odour destruction efficiency, space limitations, whether or not waste heat utilisation is practicable, and capital and operating costs.

Reineration. Non-condensable gases (and smoke from direct-fired driers) can be incinerated in a boiler firebox or in a dedicated thermal ^{reactor} (afterburner). Odorous gases must be raised to a temperature of at least 750°C for 0.5 seconds residence time with adequate oxygen ¹⁰ maximise oxidation and to minimise pyrolysis products. Adding the gas stream with boiler primary air may be practicable providing boiler oygen requirements are met, gas stream volume is not excessive, and the appliance has sufficient determined avidation will we perature/time requirements. The gas stream must not be introduced into the boiler back-end or stack - at best only partial oxidation will we have a stream must not be introduced into the boiler back-end or stack - at best only partial oxidation will the method has minimal capital and operating costs. We want the 'burnt' smell may be as objectionable as the untreated gas stream. The method has minimal capital and operating costs. However, some engineers are cautious about introducing potentially corrosive and fouling gases to boilers (pre-treatment by water scrubbing may add, some engineers are cautious about introducing potentially corrosive and fouling gases to boilers (pre-treatment by water scrubbing may add, some engineers are cautious about introducing potentially corrosive and fouling gases to boilers (pre-treatment by water scrubbing may add, some engineers are cautious about introducing potentially corrosive and fouling gases to boilers (pre-treatment by water scrubbing add, some engineers are cautious about introducing potentially corrosive and fouling gases to boilers (pre-treatment by water scrubbing). may address this concern). A better, but more costly, alternative is use of a thermal afterburner. At least one N.Z. company provides a

Tange of high destruction efficiency afterburners which can be equipped with waste heat recovery systems to pre-heat inlet gases and combustic combustion air, and to generate hot water. They have high capital cost, and generally high fuel costs unless a high degree of waste heat recovery is a state of the state of recovery is practicable.

Chemical Scrubbing. Most scrubbers used in N.Z. are either one or two stage packed tower or cross-flow units using a dilute acid first stage to remove alkaline sodium hypochlorite solution or alkaline hydrogen peroxide ¹⁰ remove ammonia and amines, followed by an oxidising stage using alkaline sodium hypochlorite solution or alkaline hydrogen peroxide solution. Most single stage scrubbers have only the oxidising stage. Scrubbers should be equipped with automatic reagent dosing systems but allow but auto-regulation of hypochlorite reagent strength at concentrations above about 200mg/litre is difficult. Generally, N.Z. rendering industru industry experience is discouraging. An excellent development (but not yet available in Australasia) is the ICI Katalco 'Odorgard' catalyst destruction efficiency and low reagent concentrations can be ^{vystem} attached to the hypochlorite stage - this significantly increases odour destruction efficiency and low reagent concentrations can be used to the hypochlorite stage - this significantly increases odour destruction air with reasonable space requirements, but their chemical scrubbers are able to treat large volumes of relatively cool gas, and ventilation air, with reasonable space requirements, but their capacity to remove smoke generated by direct-fired driers is limited. Capital cost and running costs are relatively high.

Treating non-condensable gases cooled to 40°C or less and ventilation air in an appropriately designed and maintained biological filter can achieve high odour destruction, although excessive smoke from direct-fired driers may cause problems. Current biofilters use compost, pinus radiata bark, soil and sand, or a mixture of these, to adsorb most rendering odorous contaminants for sufficient time to be Oxidised by aerobic bacteria. Media must be porous and kept damp and gas flow to media volume kept low. If too wet, increased back pressure causes problems; if too dry media contracts and develops fissures. Biofilters may be constructed below or above ground, but if above by ground walls must be gas-tight. They must have good drainage, and to avoid discharges to land the base should be impervious and hainage. drainage routed through a gas-tight trap to a receiver. Roofing the filter prevents rain water flooding and minimises drying out but adds ^{appreciably} to capital cost and limits access. Media life depends on filter construction, media type, contaminant load, and ability to maintain ^{bood} preciably to capital cost and limits access. Media life depends on filter construction, media type, contaminant load, and ability to maintain ⁸⁰⁰ moisture levels. Good quality bark should last for at least 3 years; and more if roofed. Biofilters should be equipped with pressure function) the drop indication (logged daily), and inlet gas temperature indication. If over-heating is possible (eg. through loss of condenser function) the biofilter inlet duct should be equipped with an alarm system, a heat-sensitive frangible; and/or with automatic heat source cut-out. Inlet gas the inlet duct should be equipped with an alarm system, a heat-sensitive trangitie, and of with declaring to high back pressure and the person of media by condensation leading to high back pressure and defective. defective operation. The capital cost of large biofilters is high and land area required is large, but running costs relatively low although media teplace operation. The capital cost of large biofilters is high and land area required is large are available in Europe. North America, and in ^{teplacement} must be budgeted. Proprietary multi-tiered biofilters using synthetic media are available in Europe, North America, and in Australia, but these, while being compact, are expensive.

Other Odour Control Methods.

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De odorising reagents are marketed to control odours by application as a spray on contaminated surfaces and into air. Some are claimed to reutraliant of the straight of the but neutralising compounds and masking agents (masking agents should be avoided). Some reagents appear effective especially when applied to the state of the stat applied to contaminated surfaces. There is only limited published scientific trials quantifying their effectiveness. The capital cost of spray application of the scientific trials and the scinetific trials and the scinetific trials and the scientific t applications is usually modest, and operating cost reasonable if rate of application is limited.